## CO<sub>2</sub> Geological Storage – Geotechnical Implications

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### Abstract

Fossil fuels account for more than 90% of the world total energy consumption. The emission of  $CO_2$  to the atmosphere can be reduced by the development and implementation of carbon capture and storage technologies. The geological formations considered for  $CO_2$  storage are saline aquifers, depleted and semidepleted hydrocarbon reservoirs, and unminable coal seams. The efficient short-term injection and the stable long-term geological storage of carbon dioxide are affected by complex hydro-chemo-mechanical interactions that take place in the formation, including water acidification, mineral dissolution, and stress and volume changes. Positive feedback mechanisms may lead to runaway effects. These hydro-chemo-mechanical coupled processes and emergent phenomena may hinder the storativity of injected carbon dioxide. Technological developments such as adequate geophysical tools for injection and reservoir monitoring, are needed for the safe geo-storage of  $CO_2$ .

Keywords: carbon dioxide, sustainability, geological storage, reservoir engineering, geotechnical implication, leaks

## 1. Introduction

Quality of life, in terms of education, infant mortality and life expectancy, correlates with energy consumption. Global energy consumption will increase dramatically in the next decades, and it will largely rely on fossil fuels because of the available reserves, their low cost, the investment in current infrastructure, and the still limited development of renewable energy. Currently, 90% of the total primary energy sources in the world are fossil fuels, and more than 85% in the USA (DOE, 2010).

The use of fossil fuels is intimately linked to the emission of  $CO_2$  into the atmosphere. The current concentration of  $CO_2$  in the atmosphere is ~385 ppm (parts per million), which is almost twice the concentration before the Industrial Revolution (200 ppm - IPCC, 2001). Anthropogenic  $CO_2$  global emissions add to ~7 GtC/year (see Fig. 1). The USA releases 1.59 GtC/yr and China 1.78 GtC/yr – 2007 data (CDIAC, 2009). Power plants account for ~40% of total  $CO_2$  emissions. Once released into the atmosphere,  $CO_2$  enters into the global carbon cycle and interacts with the ocean and terrestrial sinks as shown in Fig. 2.

The estimated net annual increase of  $CO_2$  concentration in the atmosphere is problematic since  $CO_2$  is a greenhouse gas. The mean surface temperature has increased ~0.6±0.2°C since the industrial revolution, and atmospheric models forecast as much as a ~3°C increase by 2100 if anthropogenic  $CO_2$  emissions

continue current trends (Fig. 3). The UN Framework Convention on climate change has suggested that the atmospheric concentration of  $CO_2$  should not exceed 450 ppm to prevent a major impact on climate conditions. Several technologies have been proposed for mitigating the emission of  $CO_2$  into the atmosphere (Table 1). Two clear options call for reducing the combustion of fossil fuels, and capturing the generated  $CO_2$  followed by permanent sequestration.

Suggested minimum storage time for CO<sub>2</sub> geological storage



Fig. 1. Annual CO<sub>2</sub> Emissions per Person as a Function of Gross Domestic Product (adjusted for inflation) for Different Countries (Data from the Carbon Dioxide Information Analysis Center (www.cdiac.ornl.gov) and (www.gapminder.org).)

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Fig. 2. Anthropogenic Perturbation of the Carbon Dioxide Cycle (Values show the annual contribution of various components (data from: Global-Carbon-Project 2010).)

ranges between 1,000 and 10,000 years. This requirement is less demanding than for nuclear waste in part due to the expectation that future technological developments might find other methods to mitigate global warming, and because of natural climate fluctuations such as the average glacial cycle period of 28,000 years (Augustin *et al.*, 2004). Figure 4 shows a comparison of time scales for different processes related to human activities and geologic processes relevant to energy. The dramatic contrast



Fig. 3. Past and Extrapolated Future CO<sub>2</sub> Emissions (data from: Pacala and Socolow 2004; World-Resources-Institute 2010a) and Global Warming Predictions for Different CO<sub>2</sub> Levels (data from: Solomon, 2007)

CO <sub>2</sub> emission mitigation technology	Advantages	Difficulties	Capacity and certainty of execution	
	DIRECT - capture, transport, and	final sequestration of $CO_2$ generated from fossil fu	el power plants	
CO <sub>2</sub> geological storage coupled or not with fuel switching	<ul> <li>Available injection technology</li> <li>Large capacity</li> <li>May give additional revenue by enhanced hydrocarbon production</li> </ul>	<ul> <li>Cost: it needs additional energy consumption ~20% for carbon capture and storage<sup>(1)</sup></li> <li>Monitoring, contamination, and liability</li> </ul>	- Large capacity: 10 <sup>3</sup> ~10 <sup>4</sup> GtCO <sub>2</sub> , mostly in saline aquifers <sup>(2)</sup>	
Ocean storage	<ul> <li>Easy and relatively inexpensive</li> <li>No porous media involved</li> </ul>	<ul> <li>Water acidification and effects on aquatic life<sup>(3)</sup></li> <li>Transportation to the site</li> </ul>	- Very large capacity $>> 10^3$ GtCO <sub>2</sub> (volume of the ocean deeper than $\sim$ 3000 m)	
Chemical carbonation	- Thermodynamically stable	- Expensive and labor intensive	- Very limited; for example: annual production of concrete is ~15 Gt concrete	
INDIRE	ECT - produce $CO_2$ - free energy, in	nprove energy conservation and efficiency, or incre	ease $CO_2$ natural uptake	
Alternative energy sources				
Renewables, Solar, Wind, Geothermal	- Almost C-free	- Small contribution to the energy portfolio	- Currently provide 4% of the energy demand <sup>(4)</sup>	
Nuclear fission	- Almost C-free - Available technology	<ul> <li>Nuclear waste</li> <li>Non-commercial use of nuclear power technology</li> </ul>	- Currently provide 6% of the energy demand <sup>(4)</sup>	
Biofuels	- Consume bio-products in excess, e.g. sugar cane and corn	- Competes with food supply	- In Brazil ethanol accounts for less than 5% of the energy production <sup>(5)</sup>	
Conservation and efficiency				
Change in people's habits - e.g. promote mass transit	- Almost no cost	- Requires time and policy	- Some countries are already highly efficient	
More efficient end-use energy technologies and appliances - HVAC	- In progress	- It needs market-transforming policies <sup>(6)</sup>	- Efficient implementation could reduce carbon emissions from the building sector to levels equivalent to those 20 years ago	
CO <sub>2</sub> surface uptake				
Terrestrial uptake	- Relatively inexpensive	<ul> <li>Difficult to increase natural sinks (trees, algae)</li> <li>Uncertainties about land use in the future<sup>(7)</sup></li> </ul>	<ul> <li>Currently at maximum</li> <li>Uptake about ~20% of total emissions</li> </ul>	

(1) (Dooley *et al.*, 2006; Heddle *et al.*, 2003); (2) (IPCC, 2005); (3) (Golomb, 1993; House *et al.*, 2006); (4) (IEA, 2009); (5) (World-Resources-Institute, 2010b); (6) (Brown and Southworth, 2008); (7) (Jaccard, 2005)



Fig. 4. Time Scales of Relevant Energy-Related Activities and Processes (Note: (1) Estimation based on the capacity of forest to absorb carbon in the atmosphere, 0.17 GtC/yr, from IPCC 2001).)

between political, engineering, and geological time scales add difficulty to short-time decision making.

The purpose of this manuscript is to explore geotechnical concepts relevant to carbon dioxide geological storage. First, we review the chemo-physical properties of water-CO<sub>2</sub>-mineral systems, reservoir conditions, and the fundamentals of CO<sub>2</sub> geological storage. Next, we explore various hydro-chemo-mechanical coupled processes that may lead to emergent phenomena and increase the probability of geotechnical hazards. Finally, we investigate potential geophysical strategies to monitor the evolution of CO<sub>2</sub> storage projects.

## 2. CO<sub>2</sub> Geological Storage and Reservoir Conditions

#### 2.1 Volume Estimation

The injected CO<sub>2</sub> displaces the original fluids that fill the voids in geological formations. The volume of the geological formation  $V_{bulk}$  affected by the injection of a volume of CO<sub>2</sub>  $V_{CO2}$  is a function of the average porosity of the reservoir *n*:

$$V_{bulk} = \frac{1}{\psi} \frac{V_{CO2}}{n} \tag{1}$$

where the displacement efficiency coefficient is  $\psi \sim 0.6$  in media with spatially correlated random porosity and can be very low  $\psi < 0.1$  if fingered invasion takes place (note: buoyancy effects, closed hydraulic boundary conditions, and the use of multiple injection wellbores can lower efficiency by as much as  $\psi \sim 0.01$ (refer to Ehlig-Economides and Economides, 2010)). Let's assume a target sequestration of 4 GtC/year (for a flat trend based on present data – Fig. 3). The total amount of CO<sub>2</sub> to be sequestered in the next 50 years is 200 GtC or 730 GtCO<sub>2</sub>. In a compressed state ( $\rho_{CO2} \sim 0.7$  tonnes/m<sup>3</sup>), this mass would occupy a volume  $V_{CO2} = 1,050$  km<sup>3</sup>. The geological volume for storage would be  $V_{bulk} \sim 27,500$  km<sup>3</sup> for a porosity  $n \sim 0.2$ , and displacement efficiency  $\psi = 0.5$ . A 100 m thick reservoir would extend  $\sim 325$  km in each direction.

#### 2.2 CO<sub>2</sub> Trapping

The trapping mechanisms to keep  $CO_2$  within deep geological formations rely on physical as well as chemical processes (Dooley *et al.*, 2006; IPCC, 2005; Jaccard, 2005). Physical trapping mechanisms include structural and stratigraphic trapping by cap rocks, hydrodynamic trapping by slow aquifer currents, and capillary trapping by interfacial forces. Chemical trapping mechanisms include dissolution of  $CO_2$  in water, mineralization,  $CO_2$  adsorption on coal and rich-organic shales, and  $CO_2$  hydrate formation. Most trapping mechanisms and safe disposal conditions are found and favored at depth. We note that there are natural accumulations of  $CO_2$  in the Earth's upper crust where  $CO_2$  has been contained for geological times such as the Ladbroke Grove and Katnook Gas Fields in southeastern Australia (Watson *et al.*, 2004).

#### 2.3 Geological Formations

Stable sedimentary basins facilitate  $CO_2$  storage, particularly when they are near emission points. These basins are found in



Fig. 5. CO<sub>2</sub> Storage Alternatives: (a) Deep Saline Aquifers, (b) Depleted Hydrocarbon Reservoirs, (c) CO<sub>2</sub>-enhanced Oil Recovery, (d) CO<sub>2</sub>-enhanced Gas Recovery from Coal Bed Methane, (e) CO<sub>2</sub>-CH<sub>4</sub> Replacement in Hydrate Bearing Sediments (Depths shown for selected pilot projects.)

most continents (IPCC, 2005). The USA, Canada and Australia have extensive storage capacity (Dooley *et al.*, 2006).

Favorable storage sites must have a thick accumulation of permeable sediments to maximize storage capacity and injectivity, overlain by a highly impermeable seal or cap rock (generally shale and evaporites).

The increase in effective stress with depth *z* leads to low porosity fine grained sediment barriers. Pore size depends on porosity and specific surface. In high specific surface montmorillonitic shales, the mean poresize can be in the order of  $10^{-8}$ m (Armitage *et al.*, 2010; Hildenbrand *et al.*, 2002). High porefluid pressure at depth also lowers the mass density difference between water and CO<sub>2</sub>, increases the solubility of CO<sub>2</sub> in water, and increases the adsorption of CO<sub>2</sub> in coal.

The geological system should be structurally simple. Candidate storage sites are assessed for reservoir size, depth and hydrogeology, geology and petrophysical characteristics of the reservoir and the seal cap rock, surface temperature and geothermal gradient, tectonic stability and faulting intensity, accessibility, infrastructure, and proximity to major  $CO_2$  sources.

Figure 5 shows schematic diagrams of various formations for  $CO_2$  geological storage. The principal targets for  $CO_2$  injection are deep saline aquifers and depleted/semidepleted hydrocarbon reservoirs (which inherently include physical barriers and cap rocks). Injection into coal seams benefits from the co-production of  $CH_4$ . Similarly, hydrate-bearing sediments can also be used to sequester  $CO_2$  while at the same time releasing  $CH_4$  (a pilot test in the Alaska North Slope is planned for 2011, US DOE-NETL, project DE-NT0006553). Deep saline aquifers are most abundant and could store 110 to 2700 GtC (Gale, 2004).

## 2.4 Pilot Projects

There are more than 50 CO<sub>2</sub> injection projects reported



Fig. 6. Pressure-Temperature Dependent CO<sub>2</sub> Phases (Pilot CO<sub>2</sub> injection projects are superimposed on this plot. Unless reported in the original sources, the PT conditions are estimated as:  $P = g \rho_w z$ ,  $T = T_0$  (4°C) + 30°C/km·z. (CO<sub>2</sub> hydrate phase boundary from Sloan and Koh 2008; Takenouchi and Kennedy, 1965).)

worldwide (NETL, 2010). Figure 6 shows the mean pressuretemperature conditions at these storage sites. Most projects involve supercritical CO<sub>2</sub> and relatively small volumes.

#### 2.5 Implementation

The injection of  $CO_2$  underground can be implemented with technology developed for petroleum and gas production. In fact, acid gas injection is routinely done in Alberta,  $CO_2$ -enhanced oil recovery is a common practice in oil reservoirs around the world, and there are more than ~5000 km of  $CO_2$  pipelines in North America (Dooley *et al.*, 2006). Still, the systematic geological storage of  $CO_2$  will require improvements in risk assessment, adequate evaluation of regional capacity and reservoir integrity, matching emission sources with sinks, and enhanced monitoring technology (Gale, 2004). In addition to these technical difficulties, economical, political, and legal obstacles have hindered the adoption of CSS technologies.

## 3. Underlying Concepts and Implications

#### 3.1 Geochemical Concepts

#### 3.1.1 Properties of CO<sub>2</sub>

The combustion of fossil fuels yields  $CO_2$  among other byproducts. For example, burning methane produces

$$CH_4 + 2O_2 \rightarrow CO_2 + 2H_2O$$
<sup>(2)</sup>

The physical properties of CO<sub>2</sub> depend on pressure-temperature P-T conditions. The CO<sub>2</sub> phase diagram is shown in Fig. 6. CO<sub>2</sub> is a gas at normal temperature and pressure, it turns into liquid at moderate pressures ~6.4 MPa at 298 K, and becomes supercritical when the temperature is higher than 304.1 K and the pressure is greater than 7.38 MPa. The mass density  $\rho$  of CO<sub>2</sub> varies widely, in fact, CO<sub>2</sub> is heavier than seawater at pressures above ~28 MPa at 277.15 K ( $\rho_{CO2}$ =1035 kg/m<sup>3</sup>). Mass density can be approximated with a cubic equation of state (Peng and Robinson, 1976) or using more accurate but complex equations (Span and Wagner,



Fig. 7. Density and Viscosity of  $CO_2$  and Water as a Function of Depth, Both on-Shore and Off-Shore (For an assumed seabed at 500 m,  $P_c$  and  $T_c$  are the critical pressure and temperature for  $CO_2$ . Note: the density of liquid  $CO_2$  exceeds the density of deep seawater when the seabed is deeper than 3000 m.)



Fig. 8. CO<sub>2</sub> Solubility in Water and pH: (a) CO<sub>2</sub> Solubility in 1 m NaCl Aqueous Solution (Note: An increase in salinity reduces CO<sub>2</sub> solubility), (b) pH as a Function of Dissolved CO<sub>2</sub> (Note: Solubility data from Duan and Sun, 2003)

1996). The mass densities of water and  $CO_2$  are plotted in Fig. 7 for typical P-T conditions present in onshore and offshore applications.

Other important P-T dependent properties of CO<sub>2</sub> include high bulk compressibility, typically an order of magnitude higher than that of water (Span and Wagner, 1996), and very low viscosity, typically 10 times lower than that of water as shown in Fig. 7,  $(\mu_{CO2}=10^{-4} \text{ Pa} \cdot \text{s at } 10 \text{ MPa} \text{ and } 280 \text{ K} - \text{Fenghour et al.}, 1998).$ 

## 3.1.2 Water-CO<sub>2</sub> Interaction and Properties

 $CO_2$  dissolves in water to form aqueous carbon dioxide  $CO_2(aq)$ . The solubility of  $CO_2$  in water  $x_{CO2}$  [mol/L] can be estimated using Henry's law

$$x_{CO2} = k_H \varphi P_{CO2} \tag{3}$$

where the Henry's coefficient is approximately  $k_H \approx 10^{-1.46} = 0.0347$  and the fugacity coefficient  $\varphi \le 1$  can be estimated with an equation of state. Water at room temperature and at 0.1 MPa contains  $x_{CO2} \approx 0.03$ -to-0.04 mol/L. That solubility increases by

two orders of magnitude  $x_{CO2} \approx 1$ -to-2 mol/L as pressure and temperature increase to reservoir conditions, i.e., one to two moles of CO<sub>2</sub> per liter of brine (Fig. 8).

Part of the aqueous carbon dioxide mixes with water to produce carbonic acid and ionizes stepwise:

$CO_2(g) \Leftrightarrow CO_2(aq)$	Henry's law	(4)
$CO_2(aq) + H_2O(l) \Leftrightarrow H^+ + HCO_3^-(aq)$	$\log K_{eq} = -6.35$ ,	
$HCO_3^{-}(aq) \Leftrightarrow H^+ + CO_3^{2-}(aq)$	$\log K_{eq} = -10.33$	3

The final result of adding CO<sub>2</sub> to water is the production of ion bicarbonates, an increase in H<sup>+</sup>, and a decrease in pH. At reservoir conditions, CO<sub>2</sub> dissolution in water yields a pH  $\approx$  3 (Fig. 8).

Other relevant properties of the water-CO<sub>2</sub> system include (a) solubility of water in liquid and supercritical CO<sub>2</sub> (~0.05 mol of water per kg of liquid CO<sub>2</sub> at 10 MPa and 285 K - Spycher *et al.*, 2003), (b) high diffusivity of water into liquid CO<sub>2</sub> (D  $\approx$  2-to-20× 10<sup>-8</sup>m<sup>2</sup>/s - at 7-25 MPa and 305±10 K - Espinoza and Santamarina, 2010), and (c) CO<sub>2</sub> hydrate formation at high pressure and low temperature (Fig. 6; Sloan and Koh, 2008).

Table 2. Mineral Reactions with CO <sub>2</sub> -Acidified Wa	ter
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Mineral	Typical reaction	Reaction rate	Notes
1) Silicates <sup>a)</sup>	$\begin{array}{l} SiO_{2(s)} + 2H_2O \Leftrightarrow H_4SiO_4 \\ \Leftrightarrow H^+ + H_3SiO_4^- \\ \Leftrightarrow H^+ + H_2SiO_4^{2} \end{array}$	1.26×10 <sup>-14</sup> mol $\cdot$ m <sup>-2</sup> s <sup>-1</sup> (White <i>et al.</i> , 2005)	• Solubility of quartz does not change with concentration of dissolved CO <sub>2</sub>
2) Aluminosilicates <sup>b)</sup>	Anorthite: CaAl <sub>2</sub> Si <sub>2</sub> O <sub>8(s)</sub> + 8H <sup>+</sup> $\Leftrightarrow$ Ca <sup>2+</sup> + 2Al <sup>3+</sup> + 2H <sub>4</sub> SiO <sub>4</sub> , K <sub>eq</sub> = 10 <sup>21.7</sup> Kaolinite: Al <sub>2</sub> Si <sub>2</sub> O <sub>5</sub> (OH) <sub>4</sub> (s) + 6H <sup>+</sup> $\Leftrightarrow$ 2Al <sup>3+</sup> + 2H <sub>4</sub> SiO <sub>4</sub> + H <sub>2</sub> O, K <sub>eq</sub> = 10 <sup>3.8</sup>	Anorthite: $1.2 \times 10^{-5} \text{ mol} \cdot \text{m}^{-2}\text{s}^{-1}$ Oligiocalse: $1.2 \times 10^{-8} \text{ mol} \cdot \text{m}^{-2}\text{s}^{-1}$ Albite: $3.6 \times 10^{-9} \text{ mol} \cdot \text{m}^{-2}\text{s}^{-1}$ Kaolinite: $10^{-14}\text{-to}-10^{-15} \text{ mol} \cdot \text{m}^{-2}\text{s}^{-1}$ (Gaus <i>et al.</i> , 2005)	<ul> <li>Include feldspars, micas, and clays.</li> <li>Reaction rate is slow.</li> <li>Yields more dissolved cations than carbonate.</li> <li>Results in pH up to 8.</li> </ul>
3) Carbonates <sup>e)</sup>	$\begin{array}{l} {\rm CaCO}_{3({\rm s})} + {\rm H}^{+} \Leftrightarrow {\rm Ca}^{2+} + {\rm HCO}_{3}^{-}, \\ {\rm K}_{\rm eq} = 10^{1.85} \\ {\rm CaCO}_{3({\rm s})} + {\rm CO}_{2} + {\rm H}_{2}{\rm O} \Leftrightarrow \\ {\rm Ca}^{2+} + 2{\rm HCO}_{3}^{-}, {\rm K}_{\rm eq} = 10^{-4.5} \\ {\rm CaCO}_{3({\rm s})} + {\rm H}_{2}{\rm O} \Leftrightarrow \\ {\rm Ca}^{2+} + {\rm HCO}_{3}^{-} + {\rm OH}^{-}, {\rm K}_{\rm eq} = 10^{-8.48} \end{array}$	Calcite: 1.6-to- $3.2 \times 10^{-5} \text{ mol} \cdot \text{m}^{-2}\text{s}^{-1}$ (Brosse <i>et al.</i> , 2005)	<ul> <li>Faster than aluminosilicates</li> <li>Solubility depends on T, P, Salinity, ionic concentration, and pH</li> <li>Dissolution rate is fast, but overall amount of reaction is small</li> <li>Results in pH from 3 to 5</li> </ul>

Sources: (a) (Drever, 1997); (b) (Li et al., 2006); (c) (Algive et al., 2009; Fredd and Fogler, 1998; Renard et al., 2005; Stumm and Morgan, 1996)



Fig. 9. Reaction Rate log ( $k_d$ / [mol/m<sup>2</sup>/s]) for Calcite CaCO<sub>3</sub>, Anorthite CaAl<sub>2</sub>Si<sub>2</sub>O<sub>8</sub>, and Kaolinite Al<sub>2</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub> at a Temperature of 40°C and [CO<sub>2(aq)</sub>] = 1 mole (For calcite,  $k_d = k_1[H^+] + k_2[H_2CO_3^*]$  where  $k_1 = 0.745$ ,  $k_2 = 8.6 \times 10^{-4}$  [mol/m<sup>2</sup>/s] at 40°C (Algive *et al.*, 2009; Fredd and Fogler, 1998; Pokrovsky *et al.*, 2005; Renard *et al.*, 2005). For anorthite,  $k_d = k_H[H^+]^{1.5} + k_{H2O} + k_{OH}[OH^-]^{0.33}$  where  $k_H = 6.883 \times 10^{-4}$ ,  $k_{H2O} = 3.58 \times 10^{-12}$ , and  $k_{OH} = 4.51 \times 10^{-14}$  [mol/m<sup>2</sup>/s] at 40°C (Li *et al.*, 2006). For kaolinite,  $k_d = k_H[H^+]^{0.4} + k_{OH}[OH^-]^{0.3}$  where  $k_H = 2.79 \times 10^{-11}$  and  $k_{OH} = 3.51 \times 10^{-16}$  [mol/m<sup>2</sup>/s] at 40°C (Li *et al.*, 2006).)

## 3.1.3 Water-CO<sub>2</sub>-Mineral Interaction

Table 2 summarizes representative chemical reactions, typical reaction rates and related comments. The equilibrium constant for dissolution reaction denotes the concentration of produced species relative to the concentration of reactant species at steady state conditions, i.e., a function of mineral solubility. The solubility of minerals in water depends on pH. (Stumm and Morgan, 1996). Furthermore, the reaction rate of minerals in CO<sub>2</sub>-water depends on temperature, pressure (i.e., CO<sub>2</sub> solubility and pH), and the concentration of other species (Algive et al., 2009; Fredd and Fogler, 1998; Pokrovsky et al., 2005; Renard et al., 2005). Dissolution rates for calcite CaCO<sub>3</sub>, anorthite CaAl<sub>2</sub>Si<sub>2</sub>O<sub>8</sub>, and kaolinite Al<sub>2</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub> are plotted as a function of pH in Fig. 9. Silicates yield more dissolved cations (pH up to 8) than carbonates (pH up to 5) but the reaction rate is much slower (Gunter et al., 2000). Consider 1 mm spheres of calcite, anorthite, and kaolinite submerged into water acidified by 1 mole of dissolved CO<sub>2</sub> per liter (pH~3). Using dissolution rates in Fig. 9 and assuming that the system is far from equilibrium, the time required to dissolve each sphere is 4 hours for calcite, 16 years for anorthite, and 226 years for kaolinite. It is also important to recognize the high reactivity of water dissolved in CO<sub>2</sub> with steel and minerals (McGrail et al., 2009).

## 3.1.4 CO<sub>2</sub> Adsorption on Organic Surfaces

Coal and organic shales adsorb  $CO_2$  (DOE-NETL, 2008; Larsen, 2004). Langmuir-type sorption isotherms are commonly used to characterize the kinetics of the reaction at pressures < 10 MPa (Ceglarska-Stefanska and Zarebska, 2002b; Mazumder, *et al.*, 2006). For reference, about ~1.6 moles of CO<sub>2</sub> can be adsorbed per kg of coal at 3 MPa and 298 K (37 cm<sup>3</sup> of gas CO<sub>2</sub> at normal pressure and temperature per gram of coal). A higher fluid pressure promotes higher and faster uptake.

#### 3.1.5 Summary

High fluid pressure and temperature bring  $CO_2$  into liquid or supercritical phases and promote  $CO_2$  solubility in water and adsorption onto organic surfaces. In the presence of  $CO_2$ , water acidifies and more intense and faster mineral dissolution takes place. Liquid and supercritical  $CO_2$  exhibit much lower viscosity than water.

#### 3.2 Mixed Fluid Conditions

#### 3.2.1 Pressure Dependent $T_s$ and $\theta$

The water-CO<sub>2</sub> interfacial tension decreases from  $T_s \sim 72$  to 25 mN/m as the pressure increases from 0.1 MPa to 6.4 MPa at  $\sim 298$  K, eventually  $T_s$  reaches a plateau at  $T_s \approx 25\pm5$  mN/m in the supercritical state (Espinoza and Santamarina, 2010; Kvamme *et al.*, 2007). Furthermore, the contact angle formed by the CO<sub>2</sub>-water interface on mineral surfaces varies with fluid pressure in response to changes in CO<sub>2</sub>-water interfacial tension: as the fluid pressure increases, the contact angle increases on non-wetting surfaces such as oil-wet quartz and coal and slightly decreases in water-wet quartz and calcite surfaces (Chalbaud *et al.*, 2009; Chi *et al.*, 1988; Chiquet *et al.*, 2007; Dickson *et al.*, 2006; Espinoza and Santamarina, 2010).

Changes in interfacial tension  $T_s$  and contact angle  $\theta$  will affect the capillary pressure, the evolution of flooding, the residual saturation, relative permeabilities, and capillary effects. In its simplest form, capillary pressure  $\Delta P_c$  [Pa] is estimated from Laplace's equation:

$$\Delta P_c = P_{CO2} - P_w = \frac{2T_s}{r} \cos\theta \tag{5}$$

#### 3.2.2 Breakthrough Pressure

The breakthrough pressure  $P_{thru}^*$  when CO<sub>2</sub> percolates through a porous medium depends on the mean pore size expressed in terms of specific surface  $S_s$  and void ratio  $e = e_{1kPa} - C_c \log(p'/1 kPa)$ , the wettability of the minerals in the presence of water and CO<sub>2</sub>, and the standard deviation in pore size distribution. We can extend Laplace's capillary pressure equation to obtain the following expression for the breakthrough pressure (Espinoza and Santamarina, 2010):

$$P_{thru}^{*} = \psi \frac{S_{s} \rho T_{s} \cos\theta}{e_{1kPa} - C_{c} \log \frac{p'}{1kPa}}$$
(6)

where p' is the in situ effective stress, and the factor  $\psi$  depends on clay fabric and grain size distribution; a value of  $0.04 < \psi < 0.08$  applies to smectite clay barriers. The sealing capacity of cap rocks will depend on this breakthrough pressure; thereafter, the leak rate will be determined by the cap rock permeability to CO<sub>2</sub> (Fleury *et al.*, 2010; Pusch *et al.*, 2010).

3.2.3 Differences in Mass Density - Convection and Self Mixing

CO<sub>2</sub> is lighter than water or brine at reservoir P-T conditions (Fig. 7). The Bond number *B* quantifies gravity-driven CO<sub>2</sub> migration as a function of the mass density difference ( $\rho_w - \rho_{CO2}$ ) relative to capillary forces  $T_s \cdot \cos\theta$  (Pennell *et al.*, 1996):

$$B = \frac{(\rho_w - \rho_{CO_2})gkk_{rCO_2}}{T_s \cos\theta} \tag{7}$$

The mass density of the water with CO<sub>2</sub> in solution  $\rho_{sol}$  [kg/m<sup>3</sup>] is slightly heavier than the formation water and can be estimated from the mass density of pure water  $\rho_w$  [kg/m<sup>3</sup>] and the concentration of CO<sub>2</sub> in water  $x_{CO2}$  [mol/m<sup>3</sup>] as:

$$\rho_{sol} = \rho_w + m_{CO2} x_{CO2} - x_{CO2} \rho_w V_\varphi \tag{8}$$

where  $m_{CO2}$ [kg/mol] is the molecular weight of CO<sub>2</sub>, and  $V_{\varphi}$  [m<sup>3</sup>/mol] is the apparent molar volume of dissolved CO<sub>2</sub> as a function of temperature T[C],  $V_{\varphi}$ =37.51·10<sup>-6</sup>-9.585·10<sup>-8</sup> T+8.740·10<sup>-10</sup>  $T^2$ -5.044·10<sup>-13</sup>  $T^3$  (Garcia, 2001). For example, there is an increase in density  $\Delta \rho \sim 10$  kg/m<sup>3</sup>, for water saturated with CO<sub>2</sub> at 10 MPa and 313K ( $x_{CO2} \sim 1230$  mol/m<sup>3</sup>). Dissolution-densification and gravity-driven flow will cause convective transport which will accelerate CO<sub>2</sub> mixing in the reservoir water (Kneafsey and Pruess, 2010; Riaz *et al.*, 2006).

#### 3.2.4 Differences in Viscosity: Fingering

Two dimensionless numbers control the pattern of fluid displacement: (1) the ratio of viscosities *M* between the invading fluid  $\mu_{CO2}$  and the displaced fluid  $\mu_w$ , and (2) the capillary number *C* which is the ratio between viscous and capillary forces:

$$M = \frac{\mu_{CO2}}{\mu_w} \tag{9}$$

$$C = \frac{q\mu_{CO2}}{T_s \cos\theta} \tag{10}$$

where  $q[m^3/s/m^2]$  is the injection rate,  $T_s[N/m]$  is the interfacial tension between water and CO<sub>2</sub>, and  $\theta$  is the contact angle formed by the water-CO<sub>2</sub> interface and the mineral surface. Stable displacement takes place when M > 1 and C > 1, viscous fingering when M << 1, and capillary fingering when C << 1 (Lenormand *et al.*, 1988). Since the viscosity of CO<sub>2</sub> is at least one order of magnitude lower than that of water at reservoir P-T conditions (Fig. 7), CO<sub>2</sub> may displace water from the pore space in the form of viscous fingers; in this case, the bulk volume of sediment  $V_{bulk}$  involved in storage will increase dramatically (Eq (1)).

## 3.2.5 CO<sub>2</sub> Lowers the Viscosity of Oil

 $CO_2$  dissolves in crude oil (typically alkanes with less than 13 carbon atoms at reservoir conditions with P > 10 MPa and T > 320 K), lowers the viscosity of the crude oil, and favors oil

recovery (Blunt et al., 1993).

### 3.2.6 Summary

Interfacial tension and the capillary entry pressure for  $CO_2$  into a water saturated seal cap rock decrease with pressure. The dissolution of  $CO_2$  in water increases the density of water, promote gravity-driven flow and accelerate mixing. Pronounced differences in viscosity between liquid or supercritical  $CO_2$  and water tend to promote viscous fingering during  $CO_2$  injection.

### 3.3 Chemo-Hydro-Mechanical Coupling

## 3.3.1 Increased Fluid Pressure and Fault Reactivation

The increase in porefluid pressure during  $CO_2$  injection can reactivate nearby faults if the state of effective stress approaches failure conditions (Rutqvist and Tsang, 2002; Streit and Hillis, 2004).

#### 3.3.2 Capillary-Driven Deformation

The invasion of immiscible  $CO_2$  in a water saturated reservoir gives rise to capillary forces and can cause significant volumetric deformation in fine-grained sediments (Delage *et al.*, 1996).

#### 3.3.3 Fluid-Driven Fracture Formation

Hydraulic fracture can take place in both cohesive-cemented and cohesionless-frictional sediments (Bjerrum *et al.*, 1972; Jaworski *et al.*, 1981; Zhai and Sharma, 2005). Particle-scale mechanisms compatible with the effective-stress dependent strength of sediments take into consideration capillary forces induced by the tensile membrane between  $CO_2$  and water, seepage drag forces, and skeletal forces to explain particle displacement and localization (Shin and Santamarina, 2010).

## 3.3.4 Effects of pH and Permittivity on Interparticle Electrical Forces - Changes in Clay Fabric

Two fluid-mineral interactions anticipate changes in interparticle forces after CO<sub>2</sub> injection: (1) water acidification changes the mineral surface charge, and (2) the low permittivity of CO<sub>2</sub> ( $\kappa^2 \sim 2$  to 3) compared to water ( $\kappa^2 = 80$ ) implies changes in van der Waal's attraction (Israelachvili, 1991; Obriot *et al.*, 1993; Palomino and Santamarina, 2005). These fluid-mineral phenomena will alter the equilibrium between van der Waal's attraction and double layer repulsion forces at the clay particle scale, cause changes in clay fabric, and affect the seal capacity of cap rocks.

#### 3.3.5 Reactive Fluid Transport - Wormholes

Acidified water dissolves minerals and enlarges pores along transport channels (Emberley *et al.*, 2004; Kaszuba *et al.*, 2005; Watson *et al.*, 2004). The hydraulic conductivity may increase by a factor of 10-to-100 (Verdon and Woods, 2007), with even small changes in global porosity, as can be predicted using the Kozeny-Carman model. Two dimensionless numbers control the evolution of dissolution patterns: Damköhler number represents the ratio between advection and reaction times  $Da=\kappa d/v$  (reaction rate

 $\kappa$ [1/s], characteristic length l[m], velocity  $\nu$ [m/s]), while the Peclet number is the ratio between advection and diffusion time  $Pe=\nu l/D$  (diffusion coefficient D[m<sup>2</sup>/s]). The process is masstransfer limited if a chemical reaction is very fast compared to mass-transfer kinetics Da>>1 (e.g., more likely in the dissolution of carbonates). Otherwise, the process is reaction-rate limited Da<<1 (e.g., more likely if the dissolution of aluminosilicates is involved). The dissolution pattern during reactive transport can be categorized as face/global dissolution ( $Da>10^{-3}$ ,  $Pe<10^{-3}$ ), dominant wormholes ( $Da>10^{-3}$ ,  $Pe>10^{-2}$ ), or uniform dissolution ( $Da<10^{-3}$ ) (Golfier *et al.*, 2002). A rapid mineral dissolution rate combines with the inherent sediment heterogeneity to facilitate a dominant wormholes tendency (Fredd and Fogler, 1998). Wormhole formation would lead to marked CO<sub>2</sub> leakage.

# 3.3.6 Dissolution - Horizontal Effective Stress $k_0$ - Shear and Tensile Fractures

Complementary analytical, numerical (DEM and FEM), and experimental techniques show the effects of mineral dissolution and ensuing particle-level volume contraction on the evolution of the state of stress under constant overburden at zero-lateral strain boundary conditions during mineral dissolution. In particular, the stress ratio at zero lateral strain  $k_0 = \sigma'_h / \sigma'_v$  (Jaky, 1944; Mayne and Kulhawy, 1982) experiences a pronounced

	Table 3.	Coupling	and	Emergent	Phenomen
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Coupling	Emergent phenomenon
Multiphase fluid phenomena	<ul> <li>Relative hydraulic conductivities</li> <li>Differences in mass density and buoyancy</li> <li>Differences in viscosity and viscous fingering</li> <li>Fluid segregation</li> <li>Pressure dependent interfacial tension and contact angle</li> <li>Percolation and breakthrough pressure</li> </ul>
Chemo-Hydro	<ul> <li>Reduction of oil viscosity by CO<sub>2</sub></li> <li>Dissolution followed by increased porosity and pore size</li> <li>Reactive transport and wormhole formation</li> <li>Spatial changes in hydraulic conductivity</li> <li>Gravity-driven self mixing, CO<sub>2</sub> diffusion, pendular water, mineral precipitation</li> <li>Coal CO<sub>2</sub> adsorption: reduced fluid conductivity and swelling pressure</li> <li>Hydrate formation and depressurization: fluid volume expansion, possible gas-driven fractures</li> </ul>
Hydro- Mechanical	<ul> <li>Increased fluid pressure and lower effective stress</li> <li>Fault reactivation; hydraulic fracture of the cap rock</li> <li>Capillarity-driven contraction</li> <li>Fluid-driven fracture formation</li> </ul>
Chemo- Mechanical	<ul> <li>pH and permittivity effects on DLVO, changes in clay fabric</li> <li>Pressure solution/precipitation</li> <li>Mineral dissolution and sediment compaction</li> <li>Cap rock bending failure</li> <li>Decrease in horizontal effective stress k<sub>0</sub> Shear fractures in contraction</li> </ul>
Chemo- Hydro- Mechanical	- Combination of previous phenomena

decrease during mineral dissolution, and it may reach the Rankine active failure condition  $k_a$  on the Coulomb failure plane (Shin and Santamarina, 2009). Strain localization along shear planes may follow (Shin *et al.*, 2008). Furthermore, mineral dissolution causes sediment compaction, and the cap rock may experience bending and tensile failure.

## 3.3.7 Coal Swelling Pressure

Coal swells, its fluid conductivity decreases, and the effective stress increases with the adsorption of CO<sub>2</sub> (Mazumder *et al.*, 2006; Pekot and Reeves, 2002; Somerton *et al.*, 1975). Eventually, CO<sub>2</sub>-CH<sub>4</sub> replacement in coal may become self-limiting because of coal swelling and reduced fracture porosity (Ceglarska-Stefanska and Zarebska, 2002a).

#### 3.3.8 Summary

The trapping mechanisms of  $CO_2$  in geological formations rely on physical, chemical, and mechanical processes identified above. Each has different time and spatial scales. We summarize potential implications on  $CO_2$  storage in Table 3.

## 4. Monitoring Strategies and Risk Assessment

 $CO_2$  leakage from storage sites back into the atmosphere decreases the efficiency of  $CO_2$  storage, may pollute drinking water aquifers and endanger living organisms. Faults and abandoned wells are preferential flow paths that add to the slow transport and diffusion through otherwise continuous strata (Dooley *et al.*, 2006; Leuning *et al.*, 2008). Monitoring is required to assess the movement of  $CO_2$  and to detect leaks. The design of a monitoring strategy must consider the large areal extent of  $CO_2$  storage reservoirs (on the order of ~km<sup>2</sup>) and account for spatial and temporal variability.

Potential monitoring methods, most of them already available for other applications, are summarized in Table 4. These monitoring methods take advantage of differences between physical properties (mass density, bulk stiffness, electrical resistivity and dielectric permittivity, and thermal characteristics), the detection of byproducts from chemical reactions, or coupled process effects such as subsidence or micro-seismicity. Tracers such as  $\delta^{13}$ C and SF<sub>6</sub> may be included in the injected CO<sub>2</sub> to facilitate detection (Leuning *et al.*, 2008). The most common subsurface geophysical methods for deep reservoir applications are based on elastic wave propagation and electrical resistivity (Kiessling *et al.*, 2010; Nakatsuka *et al.*, 2010). The following analysis expresses their applicability to CO<sub>2</sub> geological storage. The bulk modulus *B<sub>mix</sub>* of the sediment can be estimated from the Biot-Gassman equation:

$$B_{mix} = B_{sk} + \left(1 - \frac{B_{sk}}{B_g}\right)^2 \left[n\left(\frac{S_w}{B_w} + \frac{S_{CO2}}{B_{CO2}}\right) + \frac{1 - n}{B_g} - \frac{B_{sk}}{B_g^2}\right]^{-1}$$
(11)

where subindices represent the skeleton sk, the mineral that makes the grains g, the water w, and the CO<sub>2</sub>. The density of the mixture is:

#### CO<sub>2</sub> Geological Storage – Geotechnical Implications

Method	Property measured	Principle, comments and issues
	1. SUBSURFACE MONITORING	·
Porewater geochemistry <sup>(1)</sup>	CO <sub>2</sub> , HCO <sub>3</sub> <sup>-</sup> , CO <sub>3</sub> <sup>2-</sup> , DIC, major ions, pH, alkalinity, salinity, and isotopes	CO <sub>2</sub> dissolves in water and changes water geochemistry
Seismic techniques <sup>(2)</sup>	P-wave velocity and amplitude	The bulk modulus of $CO_2$ is one order of magnitude lower than that of water
Electromagnetic techniques <sup>(3)</sup>	Resistivity and electromagnetic waves	High impedance mismatch of electrical conductivity and dielectric permittivity between $CO_2$ and formation water.
Temperature signal <sup>(4)</sup>	Temperature	$CO_2$ causes non-isothermal events such as expansion induced cooling of $CO_2$ and thermal heat dissipation from $CO_2$ dissolution
Infrared monitoring <sup>(5)</sup>	Infrared absorption	CO <sub>2</sub> gas shows characteristic absorption spectrum for infrared waves.
	2. NEAR SURFACE MONITORING	
Analysis of near-surface water <sup>(6)</sup>	Isotopic composition, tracers, bulk gas composition, and DIC	$CO_2$ dissolves in water. A meaningful analysis requires a thorough understanding of the geochemical cycle at the site.
Surface analysis of soil gas <sup>(7)</sup>	Composition of gas fluxes through the soil	$CO_2$ leaks would eventually percolate through the soil. Point measurements <1 m <sup>2</sup> are accurate but they lack spatial resolution
Near surface analysis of air composition <sup>(8)</sup>	CO <sub>2</sub> concentration in the near surface by infrared gas analyzer, eddy correlation tower, and light detection and ranging measure	CO <sub>2</sub> from leaks readily mix with other atmospheric gases. Local changes in turbulence and biological sources and sinks of CO <sub>2</sub> make the identification difficult.
	3. ON-SURFACE MONITORING	·
Time-lapse 3D reflection seismic imaging <sup>(9)</sup>	P-wave velocity and amplitude	Takes advantage of low bulk modulus of $CO_2$ . It is routinely used in the petroleum industry and can track the plume subsurface movement.
Gravity (10)	Mass density	CO <sub>2</sub> is generally lighter than water
Ground displacements <sup>(11)</sup>	Subsidence and heave, vertical displacement	CO <sub>2</sub> injection alters pore pressure and effect on effective stress, and therefore strata compressibility
Surface analysis of carbon content in soil <sup>(12)</sup>	Carbon content by Inelastic Neutron Scattering INS	Increased $CO_2$ levels asphyxiate aerobic organisms.
Remote sensing of air composition <sup>(7)</sup>	CO <sub>2</sub> atmospheric concentration by hyperspectral remote sensing of vegetative stress and long open path infrared absorption	Applicable at large scales

## Table 4. CO<sub>2</sub> Monitoring Techniques

(1) (Emberley *et al.*, 2004; Gunter *et al.*, 2000; Newell *et al.*, 2008); (2) laboratory studies (Lei and Xue, 2009; Shi *et al.*, 2007; Xue *et al.*, 2005) and pilot tests (Bohnhoff *et al.*, 2010; Daley *et al.*, 2008; Daley *et al.*, 2007; Onishi *et al.*, 2009); (3) (Gasperikova and Hoversten, 2006; Nakatsuka *et al.*, 2010); (4) (Bielinski *et al.*, 2008); (5) (Charpentier *et al.*, 2009); (6) (Oldenburg *et al.*, 2003); (7) (Leuning *et al.*, 2008; Oldenburg *et al.*, 2003); (8) (Strazisar *et al.*, 2009); (9) (Arts *et al.*, 2004); (10) (Alnes *et al.*, 2008); (11) (Alnes *et al.*, 2008; Kempka *et al.*, 2008); (12) (Wielopolski and Mitra, 2010)

$$\rho_{mix} = (1 - n)\rho_s + n(S_{CO2}\rho_{CO2} + S_w\rho_w)$$
(12)

Then, the compressional  $V_P$  and shear  $V_S$  wave velocities are:

$$V_{P} = \sqrt{\left(\frac{B_{mix} + 4/3 \cdot G_{sk}}{\rho_{mix}}\right)}$$
(13)

$$V_{S} = \sqrt{\frac{G_{sk}}{\rho_{mix}}} \tag{14}$$

where  $G_{sk}$  is the shear modulus of the mineral skeleton.

The electrical conductivity of a geological formation depends on the concentration and mobility of hydrated ions in the pore fluid and the volume fraction of fluid in the formation (Santamarina *et al.*, 2001). The injection of CO<sub>2</sub> displaces the electrolyte (conductivity  $\sigma_{fl}$ ) and the formation conductivity can be estimated using the Archie's equation (Mavko *et al.*, 2009):

Vol. 15, No. 4 / April 2011



Fig. 10. Reduction of P-wave Velocity and Electrical Conductivity  $\sigma_{form} = 1/\rho_{form}$  with CO<sub>2</sub> Saturation for a Sediment with Porosity *n*=0.42 (Ratio of P-wave velocity computed with  $V_P$ (Brine) = 1540 m/s,  $V_P$ (CO<sub>2</sub>) = 268 m/s (at *T* = 40°C and P = 10 MPa),  $V_P$ (dry sediment) = 1000 m/s, and  $v_{sk}$  = 0.1. electrical conductivity computed with an exponent  $\beta$  =2 for relative saturation and porosity, and a percolation threshold  $S_{perc}$ =0.7.)

$$\sigma_{form} = \sigma_{fl} [n(S_{perc} - S_{CO2})]^{\beta}$$
(15)

where  $S_{CO2} \le S_{perc}$ , the maximum saturation of CO<sub>2</sub> at percolation. Figure 10 shows the variation of P-wave velocity  $V_P[m/s]$  and electrical conductivity  $\sigma_{form}$  as a function of the CO<sub>2</sub> saturation  $S_{CO2}$ . Because CO<sub>2</sub> is non conductive and has a much lower bulk modulus than water, both  $\sigma_{form}$  and  $V_P$  decrease as the relative saturation  $S_{CO2}$  increases. While forward predictions show a clear effect of CO<sub>2</sub> on  $V_p$  and  $\sigma_{form}$ , the inverse analysis is hindered by measurement errors and error propagation. Hence, the estimation of  $S_{CO2}$  from field measurements remains challenging.

## 5. Conclusions

- The volume of the geological formation that is affected by the injection of CO<sub>2</sub> depends on geometric boundaries, spatial variability, flow conditions and the emergence of viscous fingering.
- The physical properties of CO<sub>2</sub> such as density, viscosity, interfacial tension and bulk compressibility vary with pressure and temperature conditions, and must be properly modeled in numerical simulations of CO<sub>2</sub> geological storage.
- In particular, the CO<sub>2</sub>-water interfacial tension decreases with fluid pressure. Lower interfacial tension reduces the capillary entry pressure for CO<sub>2</sub> into a water saturated seal cap rock.
- High CO<sub>2</sub> injection pressures can induce fluid driven fractures and trigger displacements along preexisting faults.
- The solubility of CO<sub>2</sub> in water is high as reservoir pressure conditions. The density of water increases with dissolved CO<sub>2</sub> and convective self-mixing takes place.
- Water acidification in the presence of CO<sub>2</sub> enhances mineral dissolution and alters the sediment fabric when clay minerals

prevail. Silicates have a higher buffering capacity than calcite but the reaction rate is much slower.

- The evolution of dissolution and ensuing dissolution patterns depend on the interplay between the rates of advection, diffusion and dissolution. Dissolution may cause settlement, change in effective stress, and the formation of preferential channels for fluid flow, particularly in carbonates.
- The presence of CO<sub>2</sub> decreases the fluid bulk modulus, mass density, and electrical conductivity. These changes support the application of geophysical methods based on elastic and electromagnetic waves to monitor deep storage reservoirs. While forward predictions are manageable, inverse analysis is hindered by measurement difficulties and error propagation. Hence, the monitoring of CO<sub>2</sub> geological storage remains challenging.

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